
SNAP CODE:	030308
SOURCE ACTIVITY TITLE:	PROCESSES WITH CONTACT <i>Secondary Zinc Production</i>
NOSE CODE:	104.12.09
NFR CODE:	1 A 2 b
ISIC:	2420

1 ACTIVITIES INCLUDED

Zinc is produced from various primary and secondary raw materials. The primary processes use sulphidic and oxidic concentrates, while in secondary processes recycled oxidised and metallic products mostly from other metallurgical operations are employed. This chapter includes information on atmospheric emissions during the production of secondary zinc. In practice, a clear distinction of primary and secondary zinc production is often difficult, because many smelters use both primary and secondary raw materials.

Zinc production in the western world stood at about 5.2 million tonnes in 1990. Of this, 4.73 million tonnes originate from primary resources (ores), while the balance of 0.47 million tonnes is produced at the smelters from secondary raw materials (Metallgesellschaft 1994). The production of zinc in secondary smelters is increasing in various regions of the world. This increase can be as high as 5% per year in Eastern Europe. This chapter describes the methods to estimate both combustion and process emissions of atmospheric pollutants during the secondary zinc recovery from various types of zinc scrap (e.g. Barbour et al, 1978).

2 CONTRIBUTIONS TO TOTAL EMISSIONS

There are several trace metals as well as dioxins and furans which can be emitted during the secondary zinc production process. However, heavy metal emissions from this source category are not very significant on a global scale. Nriagu and Pacyna (1988) concluded that the secondary zinc production contributes well below 1 % of the total atmospheric emissions of lead, cadmium, antimony, selenium, and zinc. A similar contribution to European atmospheric emissions from secondary zinc production was estimated at the beginning of the 1980's (Pacyna, 1983). The estimated contribution of both primary and secondary zinc production to European emissions is given in Table 2.1 (Berdowski 1997). However, a secondary zinc smelter can be an important emission source on a local scale.

The contribution of emissions released from secondary zinc production to total emissions of those pollutants covered by the CORINAIR90 inventory is negligible (see Table 2.2).

Table 2.1: Contribution to total heavy metal emissions of the OSPARCOM-HELCOM-UNECE inventory for 1990 (up to 38 countries)

Source-activity	SNAP-code	Contribution to total emissions [%]							
		As	Cd	Cr	Cu	Hg	Ni	Pb	Zn
Total Zinc Production	0403zn	0	9.1	0	0	7.1	0	0.5	9.8

Table 2.2: Contribution to total emissions of the CORINAIR90 inventory (up to 28 countries)

Source-activity	SNAP-code	Contribution to total emissions [%]											
		SO ₂	NO _x	NM VOC	CH ₄	CO	CO ₂	N ₂ O	NH ₃	TSP	PM ₁₀ *	PM _{2.5} *	
Secondary Production Zinc	030308												
Typical contribution		-	-	-	-	0	-	-	-	0.002	0.003	0.003	
Highest value										0.005	0.010	0.012	
Lowest value										-	-	-	

* EU PM_{2.5} Inventory project for EU25 for the year 2000 (TNO, 2006), contribution to total national emissions, excluding agricultural soils

0 = emissions are reported, but the exact value is below the rounding limit (0.1 per cent)

- = no emissions are reported

Secondary zinc production is unlikely to be a significant source of sulphurhexafluoride (SF₆), hydrofluorocarbons (HFCs) or perfluorocarbons (PFCs), (ETC/AEM-CITEPA-RISOE 1997).

3 GENERAL

3.1 Description

A secondary zinc smelter is defined as any plant or factory in which zinc-bearing scrap or zinc-bearing materials, other than zinc-bearing concentrates (ores) derived from a mining operation, are processed (e.g. Barbour et al., 1978). In practice, primary smelters often also use zinc scrap or recycled dust as input material.

Zinc recovery involves three general operations performed on scrap, namely pre-treatment, melting, and refining. Scrap metal is delivered to the secondary zinc processor as ingots, rejected castings, flashing, and other mixed metal scrap containing zinc (US EPA, 1995).

Scrap *pre-treatment* includes sorting, cleaning, crushing and screening, sweating, and leaching. In the sorting operation, zinc scrap is manually separated according to zinc content and any subsequent processing requirements. Cleaning removes foreign materials to improve product quality and recovery efficiency. Crushing facilitates the ability to separate the zinc from the contaminants. Screening and pneumatic classification concentrates the zinc metal for further processing. Leaching with sodium carbonate solution converts dross and skimmings to zinc oxide, which can be reduced to zinc metal (US EPA, 1995).

Pure zinc scrap is *melted* in kettle, crucible, reverberatory, and electric induction furnaces. Flux is used in these furnaces to trap impurities from the molten zinc. Facilitated by agitation, flux and impurities float to the surface of the melt as dross, and are skimmed from the surface. The remaining molten zinc may be poured into moulds or transferred to the refining operation in a molten state (US EPA, 1995).

Refining processes remove further impurities from clean zinc alloy scrap and from zinc vaporised during the melt phase in retort furnaces. Molten zinc is heated until it vaporises. Zinc vapour is condensed and recovered in several forms, depending upon temperature, recovery time, absence or presence of oxygen, and equipment used during zinc vapour condensation. Final products from refining processes include zinc ingots, zinc dust, zinc oxide, and zinc alloys (US EPA, 1995).

Generally the processes used for the recycling of secondary zinc can be distinguished by the kind of raw materials employed (Rentz et al., 1996):

Very poor oxidic residues and oxidic dusts, e.g. from the steel industry, are treated in *rotary furnaces* (Waelz furnaces), producing metal oxides in a more concentrated form. These concentrated oxides (Waelz oxides) are processed together with oxidic ores in primary thermal zinc smelters, in particular Imperial Smelting furnaces which are in use for combined lead and zinc production. In this case, a clear discrimination between primary and secondary zinc production as well as between zinc and lead production is difficult.

Metallic products prior to smelting are comminuted and sieved to separate metal grains from the oxides. Afterwards the metallic products are melted in *melting furnaces*, mainly of the induction type or muffle furnaces. Finally the molten zinc is cast and in part refined to high-purity zinc in distillation columns.

In *New Jersey retorts* it is possible to process a large variety of oxidic secondary materials together with metallic materials simultaneously. For charge preparation the oxides are mixed with bituminous or gas coal, briquetted, and coked. The briquettes together with the metallic materials are charged into the retorts. The zinc vapours from the retorts are condensed by splash-condensing.

3.2 Definitions

Secondary zinc production: - production of zinc from materials other than ores.

Other definitions are covered in Sections 3.1 and 3.3.

3.3 Techniques

A *sweating furnace* (rotary, reverberatory, or muffle furnace) slowly heats the scrap containing zinc and other metals to approximately 364°C. This temperature is sufficient to melt zinc but is still below the melting point of the remaining metals. Molten zinc collects at the bottom of the sweat furnace and is subsequently recovered. The remaining scrap metal is cooled and removed to be sold to other secondary processors (US EPA, 1995).

A more sophisticated type of sweating operation involves holding scrap in a basket and heating it in a molten salt bath to a closely controlled temperature. This yields a liquid metal, which separates downwards out of the salt, and a remaining solid of the other metals still free from oxidation. By arranging for heating to a sequence of temperatures, related to the melting point of the metals or alloys involved, a set of molten metal fractions with minimum intermixture can be obtained (e.g. Barbour et al., 1978).

For zinc production in *New Jersey retorts* the zinc containing raw materials are picked up from the stockpiling area. For some raw materials a *charge preparation* is carried out, including comminution, sieving, and magnetic separation, so that a metallic and a oxidic fraction is obtained. Furthermore, for some raw materials dechlorination is necessary. The oxidic raw materials, like dusts and zinc drosses are mixed with bituminous coal. Subsequently, the mixture which contains about 40 % zinc is briquetted together with a binding agent, coked at temperatures around 800°C in an autogenous coking furnace and then charged to the New Jersey retorts together with small amounts of pure metallic materials. By heating with natural gas and CO containing waste gases, in the retorts temperatures of around 1,100°C are achieved, so that the zinc is reduced and vaporised. Subsequently, the vaporised zinc is precipitated in splash-condensers and transferred to the foundry via a holding furnace. Here the so-called selected zinc is cast into ingots. The residues from the retorts are treated in a melting cyclone to produce lead-zinc-mix oxides and slag. Figure 3.1 shows a schematic diagram for secondary zinc production using New Jersey retorts. Potential sources of particulate and heavy metal emissions are indicated. The metallic fraction from charge preparation together with other metallic materials like galvanic drosses, scrap zinc, and scrap alloys are melted. The raw zinc is then sent to a *liquation furnace* where, in a first refining step, zinc contents from 97.5 to 98 % are achieved. The melted and refined zinc is also cast into ingots (Rentz et al., 1996).

The raw materials for *Waelz furnaces* are mainly dusts and slurry from electric arc furnaces used in the steel industry, together with other zinc and lead containing secondary materials. For transferring and charging, the dustlike secondary materials are generally pelletised at the steel plant.

After mixing, the zinc and lead containing pellets, coke as reducing agent, and fluxes are charged via a charging sluice at the upper end of the slightly sloped rotary kiln. The rotation and the slope lead to an overlaid translational and rotational movement of the charge. In a counter-current direction to the charge air as combustion gas is injected at the exit opening of the furnace. At temperatures of around 1,200°C and with residence times of around 4 hours zinc and lead are reduced and vaporised. The metal vapours are reoxidised in the gas filled space of the furnace and evacuated through the charge opening together with the waste gas. In

a cleaning device, the metal oxides are collected again and as filter dust the so-called Waelz oxide with a zinc content of around 55 % and a lead content of around 10 % is generated. The Waelz oxide is subsequently charged into an Imperial Smelting furnace which is used for combined primary zinc/lead smelting. The slag from the Waelz furnace is cooled down and granulated in a water bath. Additional oil as fuel is only needed at the start-up of the furnace, while in stationary operation the combustion of the metal vapours and carbon monoxide covers the energy demand of the process (Rentz et al., 1996). A schematic representation of the Waelz process is depicted in Figure 3.2.

Secondary zinc is sometimes combined with primary material for refining. Various pyrometallurgical refining technologies can be applied, depending on the feed material and product specification. Thermal zinc refining by fractional distillation is possible in rectifying columns at temperatures around 950°C (Rentz et al., 1996).

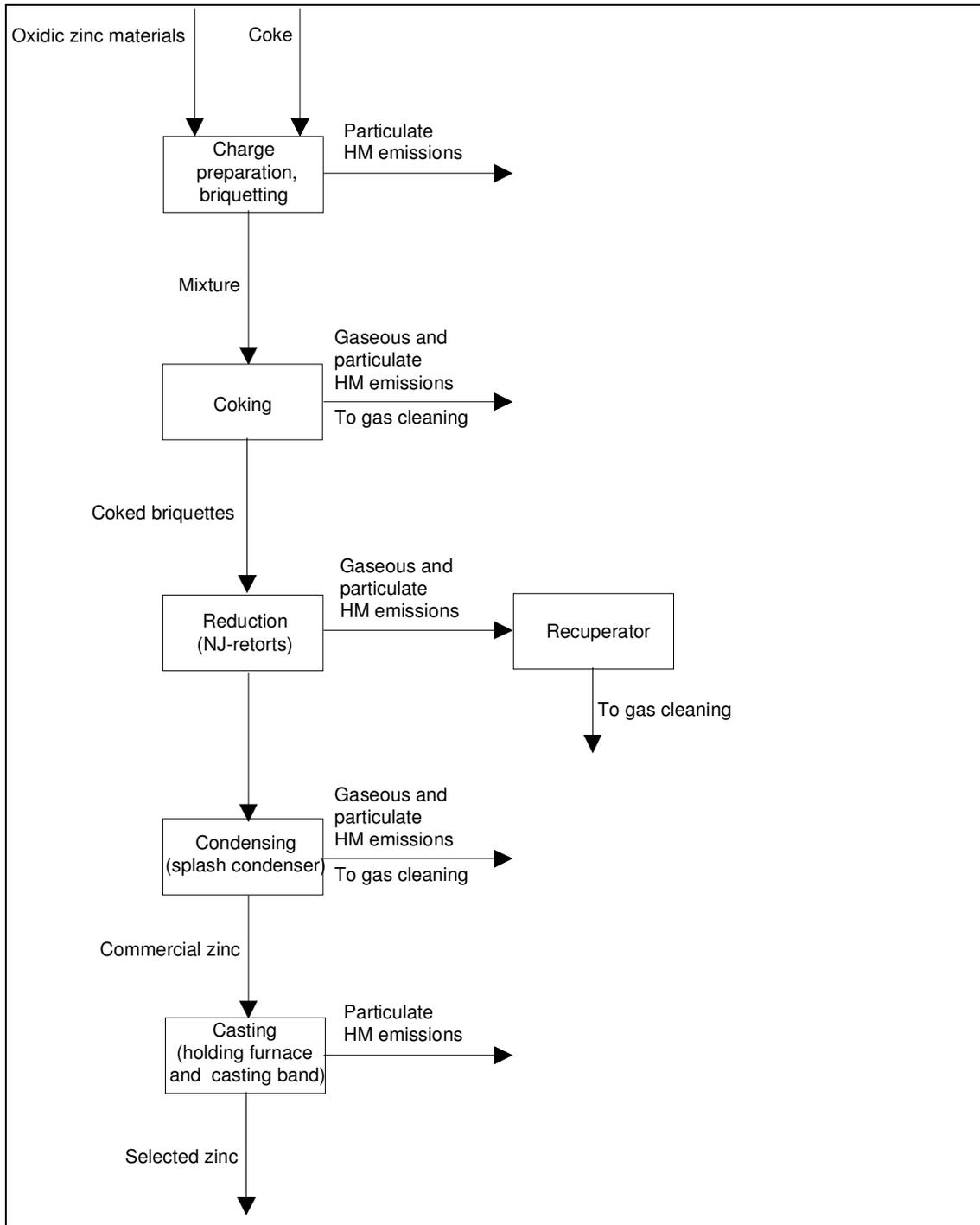


Figure 3.1: Secondary zinc production using New Jersey retorts with potential heavy metal emission sources (Rentz et al., 1996)

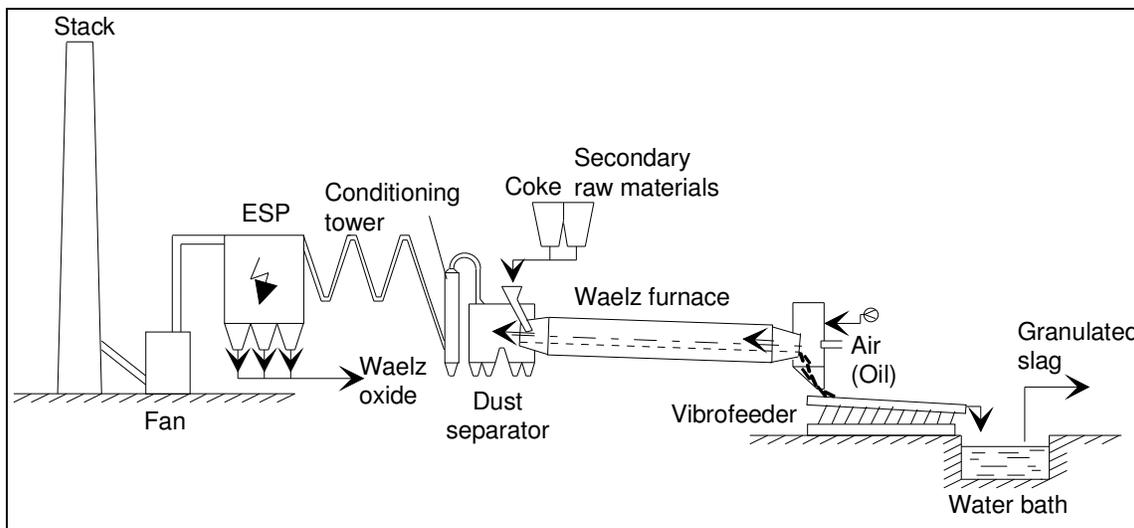


Figure 3.2: Waelz furnace with emission reduction installations (Rentz et al. 1995)

3.4 Emissions

Among the various process steps the melting furnace operation represents the most important source of atmospheric emissions. In general, continuous and periodical emissions can be distinguished. Continuous emissions are connected with the process as such, whereas periodical emissions occur e.g. during charging, heating, skimming, or cleaning operations. The most important factors influencing emissions from scrap pre-treatment and melting are:

- The composition of the raw material, in particular the content of organic and chlorinated compounds which affects the formation of dioxins and furans,
- the utilisation of flux powder ,
- the furnace type - direct heating with a mixture of process and combustion waste gases reduces the content of organic compounds released from the bath,
- the bath temperature - a temperature above 600°C creates significant emissions of zinc oxide,
- the fuel type - in general, natural gas or light fuel oil are used.

Continuous emissions from the melting furnace consist of combustion waste gases and gaseous effluents from the bath. The specific gas flow amounts to about 1,000 m³ (STP)/Mg zinc produced.

Important periodical emissions often occur with charging and melting of the raw material. Emissions of organic compounds are mainly connected with charging operations. Furnace clearing, fluxing, ash drawing, and also cleaning operations are of minor relevance. Tapping is carried out at low temperature and therefore, no metal vapours are released.

In zinc distillation a high quality input material is used and therefore, emissions of carbon or chlorine containing compounds are low. Emissions mainly consist of zinc and zinc oxide containing particles and combustion waste gases (R. Bouscaren et. al., 1988).

3.5 Controls

Most of the secondary zinc smelters are equipped with dust removing installations, such as baghouses. In general, emission control systems vary depending on the type of scrap being processed and the products being obtained. A distinction can be made between purely oxidised, mixed oxidised/metallic and purely metallic products.

The control efficiency of dust removing installations is often very high reaching 99.9 %. Both, primary gases and fugitive dust emissions are reduced in baghouses to concentrations below 10 mg/m³.

Afterburners are reported for non-ferrous-metal industry in the USA. Also wet scrubbers may be used.

4 SIMPLER METHODOLOGY

Emissions can be estimated at different levels of complexity; it is useful to think in terms of three tiers¹:

- Tier 1: a method using readily available statistical data on the intensity of processes (“activity rates”) and default emission factors. These emission factors assume a linear relation between the intensity of the process and the resulting emissions. The Tier 1 default emission factors also assume an average or typical process description.
- Tier 2: is similar to Tier 1 but uses more specific emission factors developed on the basis of knowledge of the types of processes and specific process conditions that apply in the country for which the inventory is being developed.
- Tier 3: is any method that goes beyond the above methods. These might include the use of more detailed activity information, specific abatement strategies or other relevant technical information.

By moving from a lower to a higher Tier it is expected that the resulting emission estimate will be more precise and will have a lower uncertainty. Higher Tier methods will need more input data and therefore will require more effort to implement.

For the simpler methodology (equivalent to Tiers 1 and 2), where limited information is available, a default emission factor can be used together with production capacity information for the country or region of interest without further specification on the type of industrial technology or the type and efficiency of control equipment.

Consequently the simplified methodology is to combine an activity rate (AR) with a comparable, representative, value of the emissions per unit activity, the emission factors (EF). The basic equation is:

$$\text{Emission} = \text{AR} \times \text{EF}$$

¹ The term “Tier” is used in the 2006 IPCC Guidelines for National Greenhouse Gas Inventories and adopted here for easy reference and to promote methodological harmonization.

In the energy sector, for example, fuel consumption would be activity data and mass of material emitted per unit of fuel consumed would be a compatible emission factor.

NOTE: The basic equation may be modified, in some circumstances, to include emission reduction efficiency (abatement factors).

Default emission factors for this purpose are provided in Section 8.1.

5 DETAILED METHODOLOGY

The detailed methodology (equivalent to Tier 3), to estimate emissions of gaseous pollutants from the secondary zinc production is based on measurements or estimations using plant specific emission factors - guidance on determining plant specific emission factors is given in Measurement Protocol Annex.

In this case, specific emission factors for the different process steps of the various production technologies should be used. An account of the effect of emission controls should be considered. The different emission factors will have to be evaluated through measurements at representative sites.

6 RELEVANT ACTIVITY STATISTICS

In many metal statistics secondary zinc production is not reported separately. The World Metal Statistics Year Book published by the World Bureau of Metal Statistics in Massachusetts, USA, reports total production of zinc without disaggregating it into primary and secondary production. The World Metal Statistics published monthly by the same organisation reports more detailed data which includes primary and secondary production for some countries and total production for others.

Information is also available from the UN statistical yearbooks (e.g. United Nations 1993). These data are satisfactory to estimate emissions using the simpler methodology.

The detailed methodology (tier 3) requires more detailed information. For example, the quantities of secondary zinc produced by various types of industrial technologies employed in the secondary zinc industry at plant level. This data is however not always easily available. For example, the quantities of secondary zinc produced by various types of industrial technologies employed in the secondary zinc industry at plant level. Therefore, the application of the detailed estimation methodology may be complicated unless the statistical data are available directly from a given smelter. Some information in this respect is available from the International Lead and Zinc Study Group (www.ILZSG.org).

Further guidance is provided in the 2006 IPCC Guidelines for National Greenhouse Gas Inventories, volume 3 on Industrial Processes and Product Use (IPPU), chapter 2.2.1.3 "Choice of activity statistics".

7 POINT SOURCE CRITERIA

Secondary zinc smelters should be regarded as point sources if plant specific data are available.

8 EMISSION FACTORS, QUALITY CODES AND REFERENCES

In the literature only emission factors for the simpler methodology are currently available. The CORINAIR methodology requires the separate reporting of combustion related emissions (SNAP 030308) and process related emissions (SNAP 040300). Table 8.1 also gives emission factors related to the energy input in [g/GJ] based on CORINAIR90 data. In the case of using production statistics the specific energy consumption (e.g. GJ/Mg product) has to be taken into account, which is process and country specific. Within CORINAIR 90 a value for the specific energy consumption of 38.5 GJ/Mg product was reported.

Currently, a uniform emission factor for dioxin emissions from secondary zinc production cannot be given due to the enormous range of concentrations measured in the waste gases of 6 orders of magnitude. This is illustrated by results from measurements at German plants given in Tables 8.1 and 8.3 (Quaß 1997).

Table 8.1: Emission factor table for secondary zinc production

Compound	Plant type	Emission factor	Data Quality	Abatement type	Abatement efficiency	Fuel type	Country or region	Ref.
SO ₂	<i>unknown</i>	0.85 g/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>natural gas</i>	<i>Europe</i>	<i>CORINAIR90</i>
SO ₂	Calcining kiln	9,150g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
SO ₂	Retort distillation/ oxidation	10,000g/Mg zinc oxide produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
SO ₂	Muffle distillation/ oxidation	20,000g/Mg zinc oxide produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
SO ₂	Secondary metal production, process heaters	17,209 · S g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 204, S = sulphur content of fuel	<i>USA</i>	<i>US EPA (1990)</i>
SO ₂	Secondary metal production, process heaters	19,006 · S g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 203, S = sulphur content of fuel	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	<i>unknown</i>	27 g/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>coke oven coke</i>	<i>Europe</i>	<i>CORINAIR90</i>
NO _x	<i>unknown</i>	60 g/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>natural gas</i>	<i>Europe</i>	<i>CORINAIR90</i>
NO _x	Pot furnace	950 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	Galvanising kettle	200 g/Mg zinc used	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	Rotary sweat furnace	100 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	Retort distillation / oxidation	3,950 g/Mg zinc oxide produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	Muffle distillation/ oxidation	55,000 g/Mg zinc oxide produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	Process heaters in secondary metal production	2,397 g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 204	<i>USA</i>	<i>US EPA (1990)</i>
NO _x	Process heaters in secondary metal production	6,591 g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 203	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Calcining kiln	30 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Concentrate dryer	2 g/Mg processed	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Sweating furnaces (general) Kettle (pot) melting furnace	1,200 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Crucible melting furnace, scrap smelting	1,250 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Reverberatory melting furnace, scrap smelting	2,600 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Electric induction melting furnace, scrap melting	90 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Process heaters in primary metal production	24 g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 204	<i>USA</i>	<i>US EPA (1990)</i>

PROCESSES WITH CONTACT

Activity 030308

ic030308

Table 8.1: continued

VOC	Process heaters in primary metal production	34 g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 203	<i>USA</i>	<i>US EPA (1990)</i>
VOC	Process heaters in primary metal production	44,851 g/m ³ fuel	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	NAPFUE 301, process gas	<i>USA</i>	<i>US EPA (1990)</i>
CO	<i>unknown</i>	535 g/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>coke oven coke</i>	<i>USA</i>	<i>US EPA (1990)</i>
CO	<i>unknown</i>	7 g/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>natural gas</i>	<i>Europe</i>	<i>CORINAIR90</i>
CO ₂	<i>unknown</i>	105 kg/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>coke oven coke</i>	<i>Europe</i>	<i>CORINAIR90</i>
CO ₂	<i>unknown</i>	55 kg/GJ	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>natural gas</i>	<i>Europe</i>	<i>CORINAIR90</i>
As	<i>unknown</i>	10 (1-20) g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany (1980s)</i>	PARCOM/ ATMOS (1992)
Cd	<i>unknown</i>	25 (2-50) g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany (1980s)</i>	PARCOM/ ATMOS (1992)
Cd	<i>unknown</i>	14 g/Mg zinc produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Poland</i>	S. Hlawiczka (1995)
Hg	<i>unknown</i>	0.02 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany (1980s)</i>	PARCOM/ ATMOS (1992)
Pb	<i>unknown</i>	85 g/Mg zinc produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Poland</i>	S. Hlawiczka (1995)
Pb	<i>unknown</i>	200 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany (1980s)</i>	PARCOM/ ATMOS (1992)
Zn	<i>unknown</i>	5,000 g/Mg product	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany (1980s)</i>	PARCOM/ ATMOS (1992)
Zn	<i>unknown</i>	9,000 g/Mg zinc produced	<i>E</i>	<i>uncontrolled</i>	<i>0 %</i>	<i>n. a.</i>	<i>Europe</i>	PARCOM/ ATMOS (1992)
Zn	<i>unknown</i>	1,089 g/Mg zinc produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Poland</i>	S. Hlawiczka (1995)
Zn	<i>unknown</i>	10,000 g/Mg zinc produced	<i>E</i>	<i>n. a.</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Europe</i>	R. Bouscaren (1988)
PCDD/F	<i>Hot briquetting plant capacity 16.7 Mg Zn/h</i>	63.1-379 µg I-TEQ/Mg zinc produced	<i>E</i>	<i>controlled</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany</i>	Quaß (1997)
PCDD/F	<i>Rotating cylinder (Waelz furnace), plant capacity 16.7 Mg Zn/h</i>	62.3 µg I-TEQ/Mg zinc produced	<i>E</i>	<i>controlled</i>	<i>n. a.</i>	<i>n. a.</i>	<i>Germany</i>	Quaß (1997)

n. a.: not available

Table 8.1: continued

Compound	Plant type	Emission factor	Uncertainty factor*	Abatement type	Abatement efficiency	Fuel type	Country or region	Ref.
TSP	Conventional plant	0,5 kg / Mg zinc produced	5	ESP, settlers, scrubbers; moderate control of fugitive sources	n.a.	n.a.	Europe	CEPMEIP
TSP	Modern plant (BAT)	0,5 kg / Mg zinc produced	3	fabric filters for most emission sources	n.a.	n.a.	Europe	CEPMEIP
TSP	Older plant	0,5 kg / Mg zinc produced	10	limited control of fugitive sources	n.a.	n.a.	Europe	CEPMEIP
PM ₁₀	Conventional plant	0,4 kg / Mg zinc produced	5	ESP, settlers, scrubbers; moderate control of fugitive sources	n.a.	n.a.	Europe	CEPMEIP
PM ₁₀	Modern plant (BAT)	0,4 kg / Mg zinc produced	3	fabric filters for most emission sources	n.a.	n.a.	Europe	CEPMEIP
PM ₁₀	Older plant	0,4 kg / Mg zinc produced	10	limited control of fugitive sources	n.a.	n.a.	Europe	CEPMEIP

PROCESSES WITH CONTACT

Activity 030308

ic030308

Table 8.1: continued

Compound	Plant type	Emission factor	Uncertainty factor*	Abatement type	Abatement efficiency	Fuel type	Country or region	Ref.
PM _{2.5}	Conventional plant	0,3 kg / Mg zinc produced	5	ESP, settlers, scrubbers; moderate control of fugitive sources	n.a.	n.a.	Europe	CEPMEIP
PM _{2.5}	Modern plant (BAT)	0,3 kg / Mg zinc produced	3	fabric filters for most emission sources	n.a.	n.a.	Europe	CEPMEIP
PM _{2.5}	Older plant	0,3 kg / Mg zinc produced	10	limited control of fugitive sources	n.a.	n.a.	Europe	CEPMEIP

NOTE: The uncertainty range (95% confidence) in the emission factor is expressed as a factor. The lower limit of the uncertainty range can be found by dividing the emission factor by the uncertainty factor, whereas the upper limit of the uncertainty range can be found by multiplying the range with the uncertainty factor. Example (first row in Table 8.1 on this page): The uncertainty in the emission factor for PM_{2.5} from a conventional secondary zinc production plant is 5. The emission factor with uncertainty range will therefore be 0.3 kg/Mg zinc produced with an uncertainty range of 0.06 (0.3/5) to 1.5 (0.3x5).

Table 8.2: Heavy metal emission measurements

Process type:	<i>New Jersey retorts Process waste gases</i>	Waelz furnace Process waste gases, metal oxide recovery	Waelz furnace Furnace mouth
Country or region:	Germany	Germany	Germany
Abatement:	<i>Recuperator, heat exchanger, cooler, flat bag filter (polyacrylonitrile)</i>	<i>Dust separator, conditioning tower, 3- field electrostat. precip.</i>	<i>Bag filter (Nomex needlefelt)</i>
Waste gas stream: [m ³ (STP)/h]	124,000	62,000	9,200
Compound:	<i>Clean gas [mg/m³(STP)]</i>	<i>Clean gas [mg/m³(STP)]</i>	<i>Clean gas [mg/m³(STP)]</i>
<i>As</i>	0.0009	n. a.	n. a.
<i>Cd</i>	0.02	0.014	< 0.001
<i>Cr</i>	n. a.	n. a.	n. a.
<i>Cu</i>	< 0.0009	n. a.	n. a.
<i>Hg</i>	< 0.0009	n. a.	n. a.
<i>Ni</i>	n. a.	n. a.	n. a.
<i>Pb</i>	0.11	0.4	1.3
<i>Zn</i>	n. a.	1.6	3.4
<i>Particulates</i>	6.3	5.7	8
Reference:	Steinmann (1984)	Kola (1991)	Kola (1991)

n. a.: not available

Table 8.3: PCDD/F emission measurements

Country or region:	Germany	
Process type	PCDD/F concentration waste gas [ng I-TEQ/m ³]	Mass flow [µg I-TEQ/h]
<i>Hot briquetting</i>	20 - 120	1054 - 6326
<i>Rotating cylinder</i>	20.8	1040
<i>Ore roasting furnace</i>	0.0018	
<i>Zinc melting furnace</i>	0.042 - 0.121	0.9 - 2.7
<i>Zinc melting furnace</i>	0.097	5.2
<i>Zinc melting furnace</i>	0.028	0.3
Reference:	Bröker (1995)	

9 SPECIES PROFILES

At present little information exists on physical and chemical species of trace metals and dioxins/furans emitted during the secondary zinc production. Atmospheric emissions of various pollutants depend greatly on the degree of pre-sorting and the type and homogeneity of the scrap charged. Particles emitted during the production process contain predominantly zinc oxide, some metallic zinc, chlorides of various compounds, as well as the impurities derived from other metals in the scrap charge (Rentz et al., 1996). ZnCl₂ containing particulates result from the use of fluxes and granulated metal recovered from galvanic processes as a raw material. ZnO is formed from the reaction of zinc vapour with oxides at the surface. (R. Bouscaren et al., 1988).

10 UNCERTAINTY ESTIMATES

It is difficult to assess current uncertainties of emission estimates for pollutants emitted during the secondary zinc production. Recently it was concluded that up to 50 % of uncertainties can be assigned for the emission estimates of most of the trace elements emitted from major point sources in Europe (Pacyna, 1994). Much bigger uncertainty can be assigned for emission estimates of these compounds from the secondary zinc production. Information on emission factors and statistics is largely missing for the secondary zinc smelters; thus the accuracy of emission estimates for this category cannot even be compared with the accuracy of emission estimates for major point sources, such as primary smelters and power plants.

A key uncertainty is the type of abatement associated with the emission factors in section 8 which is currently not known.

Uncertainty is also increased by missing information on secondary zinc production in activity statistics. If activity rates related to the energy input are required a conversion of units is often necessary which may cause a further increase of uncertainty.

11 WEAKEST ASPECTS/PRIORITY AREAS FOR IMPROVEMENT IN CURRENT METHODOLOGY

Development of emission factors for trace elements and dioxins/furanes and improvement of zinc emission factors given in section 8 is necessary in order to obtain emission estimates for the secondary zinc production. Further work is required to assess the missing parameters such as abatement type and efficiencies. The improvement should also focus on preparing individual emission factors for major industrial technologies and process units currently employed in the zinc industry. In this way a detailed methodology for emission estimates can be applied. Obviously, it will be necessary to obtain relevant statistical data on the production of zinc in various secondary zinc furnaces.

In many cases, a clear distinction between primary and secondary zinc production is not possible due to the simultaneous use of primary and secondary raw materials. In addition, a combined production of lead and zinc may occur (e. g. in IS-furnaces). Here, a double counting of emissions has to be avoided. Therefore, emissions from smelters should be reported as point sources using plant specific activity data.

The fuel specific emission factors cited from the CORINAIR90 inventory in Table 8.1 are related to both point sources and area sources without specification. It is assumed that according to the CORINAIR methodology they only include emissions from combustion (SNAP 030308). Further investigations should cover the influence of fuel characteristics and process technology on these factors for an improved discrimination between combustion and process related emissions.

12 SPATIAL DISAGGREGATION CRITERIA FOR AREA SOURCES

National emission estimates can be disaggregated on the basis of production, population or employment statistics.

13 TEMPORAL DISAGGREGATION CRITERIA

The secondary zinc production is a continuous process. No temporal disaggregation is needed.

14 ADDITIONAL COMMENTS

No additional comments.

15 SUPPLEMENTARY DOCUMENTS

No supplementary documents are required.

16 VERIFICATION PROCEDURES

Estimated emission factors could be best verified by measurements at plants using different industrial technologies.

17 REFERENCES

Barbour A.K., Castle J.F., and Woods S.E. (1978) Production of non-ferrous metals, Industrial Air Pollution Handbook, A. Parker (ed.), Mc Graw-Hill Book Comp. Ltd., London.

Berdowski J.J.M., Baas J., Bloos J.P.J. and Visscheldijk A.J.H (1997) The OSPARCOM-HELCOM-UNECE Emission Inventory of Heavy Metals and Persistent Organic Pollutants for 1990, TNO-MEP, Apeldoorn, the Netherlands

Bouscaren R., and Houllier C. (1988) Réduction des émissions de métaux lourds et de poussières, Technologies-efficacité-coûts, Tome 2, Métallurgie, Commission des Communautés européennes, Direction générale environnement, protection des consommateurs et sécurité nucléaire, 85-B6642-11-010-11-N

Bröker G., Bruckmann P., Geueke K.-J., Hiester E., Hoffmann, Radermacher L., and Gliwa H. (1995) "Dioxinmeßprogramm Nordrhein-Westfalen" Final report, Landesumweltamt Nordrhein-Westfalen (Ed.), 102 p.

ETC/AEM-CITEPA-RISOE (1997) Selected nomenclature for air pollution for CORINAIR94 inventory (SNAP 94), version 0.3 (Draft).

Hlawiczka S., Zeglin M., and Kosterka A. (1995) Heavy metals emission to the air in Poland for years 1980 - 1992, Inst. Ecol. Ind. Areas, Report 0-2.081, Katowice (in Polish)

ILZSG (1985) World Directory: Secondary Lead Plants, International Lead and Zinc Study Group Report, London.

Kola R., Estel R., and Steil, H. U. (1991) Abscheidung bleihaltiger Staube mit einem Ionisationswascher, Investitionen zur Verminderung von Umweltbelastungen, Programm des Bundesministers fur Umwelt, Naturschutz und Reaktorsicherheit, Luftreinhalteung, Nr. 1108

Metallgesellschaft AG (1994) The World of Metals - Zinc, Volume 2, 1st Edition 1994, ISSN 0943-3511

van der Most P., and Veldt C. (1992) Emission Factors Manual PARCOM-ATMOS, Emission factor for air pollutants 1992, Ref.-No. 92-235

Nriagu J.O. and Pacyna J.M. (1988) Quantitative assessment of worldwide contamination of air, water and soils by trace metals. *Nature*, 333, 134-139.

Pacyna J.M. (1983) Trace element emission from anthropogenic sources in Europe. Norwegian Institute for Air Research, NILU Rept. TR 10/82, Lillestrom, Norway.

Pacyna J.M. (1989) Technological parameters affecting atmospheric emissions of trace elements from major anthropogenic sources, J.M. Pacyna and B. Ottar, eds., *Control and Fate of Atmospheric Trace Metals*, Kluwer Academic Publ., Dordrecht, the Netherlands.

Pacyna J.M. (1994) Emissions of heavy metals in Europe, Background Document for the EMEP Workshop on European Monitoring, Modelling and Assessment of Heavy Metals and Persistent Organic Pollutants, Beekbergen, the Netherlands, 3-6 May, 1994.

Qua U. (1997) Landesumweltamt Nordrhein-Westfalen, Personal communication

Rentz O., Puchert H., Penkuhn T., and Spengler T.(1995) Stoffstrommanagement in der Eisen- und Stahlindustrie, Konkretisierung des § 5 Abs. 1 Nr. 3 Bundes-Immissionsschutzgesetz, Umweltforschungsplan des Bundesministers fur Umwelt, Naturschutz und Reaktorsicherheit, Luftreinhalteung, Forschungsbericht 95-104 06 001

Rentz O., Sasse, H., Karl, U., Schleef, H.-J., and Dorn, R.(1996) Emission Control at Stationary Sources in the Federal Republic of Germany, Volume II, Heavy Metal Emission Control, Umweltforschungsplan des Bundesministers fur Umwelt, Naturschutz und Reaktorsicherheit, Luftreinhalteung, 104 02 360

Steinmann U. (1984) Verminderung der Emissionen Zinkarbeit des Huttenwerkes, Altanlagenprogramm des Bundesministers des Inneren, Luftreinhalteung, Nr. 1065

United Nations (1993) *Industrial Statistics Yearbook 1991*, Vol. II, Commodity Production Statistics, New York

US EPA (1990) AIR Facility Subsystem, EPA-Doc. 450/4-90-003, Research Triangle Park.

US EPA (1995) *Compilation Of Air Pollutant Emission Factors*, Volume I, Fifth Edition, AP-42

Visschedijk, A.J.H., J. Pacyna, T. Pulles, P. Zandveld and H. Denier van der Gon, 2004, Coordinated European Particulate Matter Emission Inventory Program (CEPMEIP), In: P. Dilara et. Al (eds), *Proceedings of the PM emission inventories scientific workshop*, Lago Maggiore, Italy, 18 October 2004, EUR 21302 EN, JRC, pp 163 - 174

18 BIBLIOGRAPHY

UN ECE State-of-the-Art Report on the Heavy Metals Emissions, the UN ECE Task Force on Heavy Metals Emissions, Prague, the Czech Republic, June 1994.

US EPA (1995) Compilation Of Air Pollutant Emission Factors, Volume I, Fifth Edition, AP-42

Rentz O., Sasse, H., Karl, U., Schleef, H.-J., and Dorn, R.(1996) Emission Control at Stationary Sources in the Federal Republic of Germany, Volume II, Heavy Metal Emission Control, Umweltforschungsplan des Bundesministers für Umwelt, Naturschutz und Reaktorsicherheit, Luftreinhalteung, 104 02 360.

19 RELEASE VERSION, DATE AND SOURCE

Version : 2.1

Date : 1 February 1999

Updated by: Otto Rentz, Ute Karl
University of Karlsruhe (TH)
Germany

Updated with emission factors (CEPMEIP) for particulates by:
Tinus Pulles and Wilfred Appelman
TNO
The Netherlands
May, 2006

Original author: Jozef M Pacyna
Norwegian Institute for Air Research (NILU)
Norway

With support from: Otto Rentz, Dagmar Oertel
University of Karlsruhe (TH)
Germany

20 POINT OF ENQUIRY

Any comments on this chapter or enquiries should be directed to:

Ute Karl

French-German Institute for Environmental Research
University of Karlsruhe
Hertzstr 16
D-76187 Karlsruhe

PROCESSES WITH CONTACT

Activity 030308

ic030308

Germany

Tel: +49 721 608 4590

Fax: +49 721 75 89 09

Email: ute.karl@wiwi.uni-karlsruhe.de