

Category		Title
NFR	5.B.2	Biological treatment of waste – anaerobic digestion at biogas facilities
SNAP	091006	Biogas production
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1 Overview

This chapter covers the emissions from the biological treatment of waste by anaerobic digestion at biogas facilities. Feedstocks for anaerobic digestion can be any biodegradable organic material such as livestock manure and crops from agriculture, food waste from food processing industries, households and restaurants, and organic waste from municipalities. The 2014 nomenclature for reporting (NFR), used for the international reporting of emission inventory data, introduced the new source category '5.B.2 Biological treatment of waste — anaerobic digestion at biogas facilities'.

2 Description of sources

2.1 Process description

Anaerobic digestion is a natural process by which biomass is broken down by naturally occurring microorganisms in the absence of oxygen. These microorganisms digest the biomass and release a methane-rich gas (biogas) that, if collected in a biogas plant, can be used to generate renewable heat and power. The remaining material (digestate) is rich in nutrients, so it can be used as a fertiliser.

The digestion process depends on the biomass of microbes, the substrate composition, the temperature in the digester, the dry matter content of the feedstock and the residence time in the digester. Depending on the digestion technique and in order to improve the digestion process, feedstock pre-treatment and mixing of feedstock can be useful.

2.2 Techniques

Technologies developed to digest biomass fall into the following categories:

- 1. wet or low solid digestion: operated at a dry matter content of less than 10 % (but the feedstock can have much higher solid content, which would dilute upon entry);
- 2. dry or high solid digestion: operated at between a 15 % and 35 % dry solid content;
- 3. two- or multi-stage digestion: the development of multi-stage processes aimed to improve different stages of the digestion process, thus providing flexibility and better process control for the different stages of the anaerobic biochemical reactions.

The general concept of a biogas facility comprises the following stages:

- 1. pre-storage of feedstock
- 2. anaerobic digestion in the digester
- 3. separation of the digestate
- 4. storage of the digestate.

In practice, not all feedstock is stored before anaerobic digestion, but may be fed directly into the digester. The digester can consist of more than one gas-tight vessel. The storage of the digestate can be in a gas-tight vessel, an open tank or another storage facility. The storage may be combined with, or preceded by, treatment of the digestate, e.g. the separation of the liquid and solid fractions before storage. The possible treatment of the liquid fraction in a wastewater treatment

plant, the combustion of the solid fraction and the utilisation of digestate as organic fertiliser are beyond the scope of Chapter 5.B.2 (see section 2.3).

2.3 Emissions

The storage of feedstock and digestate in open tanks, as well as their mechanical treatment, may cause emissions of ammonia (NH₃) and nitric oxide (NO), as well as odour and dust. Anaerobic digestion is carried out in gas-tight vessels, and fugitive air emissions are unlikely to occur except during transfer to and from the digester and storage of feedstocks and digestate. However, fugitive emissions of biogas are possible from emergency vent valves and from poorly sealed water traps.

The emissions generated by the combustion of the biogas are addressed separately in Chapter 1.A.1.

This chapter (Chapter 5.B.2) considers the potential for NH₃ emissions from the following sources of biogas facilities:

- 1. during storage of feedstock on the premises of the biogas facility (¹);
- 2. during the liquid-solid separation of the digestate;
- 3. during storage of the digestate.

Agricultural crops used for biogas production (energy crops) are commonly stored as silage. As the pH of silage is low for conservation purposes, NH₃ emissions resulting from the storage of energy crops before anaerobic digestion are negligible.

As the digester is completely enclosed, no NH₃ emissions should occur. In the operation of a biogas plant however, instances of excess pressure might occur. In these cases, pressure valves might release some biogas (approximately 1 % of gas produced). For greenhouse gas calculations, these losses are relevant, as about 60 % of the gas volume is methane. The concentration of NH₃ in biogas is far lower (0.1–1 %), depending on the substrates being fermented. For most digestion processes, the leakage losses will therefore be less than 0.05 % of the nitrogen (N) content of the resulting digestate. Therefore, this source is considered negligible.

Most, but not necessarily all, of the digestate is used as organic fertiliser in agriculture. NH₃ emissions from utilisation in agriculture are considered in Chapter 3.D under 3.D.a.2.c. NH₃ emissions from other types of utilisation have to be reported elsewhere (e.g. in Chapter 1.A in case of incineration of the solid fraction).

Emissions of NO as well as odour and dust from anaerobic digestion at biogas facilities are not considered because of the lack of proper methodology.

2.4 Controls

Information on ways to reduce NH₃ emissions during storage of livestock manures is provided in Chapter 3B (e.g. rigid covers can reduce NH₃ emissions from storage of livestock slurry by about 80 %). No data are available on controlling emissions of NH₃ from storage of food wastes, but these are likely to be very small. The process of anaerobic digestion leads to elevated pH values and total

⁽¹⁾ NH₃ emissions from feedstock storage prior to the pre-storage on the premises of the biogas facility (e.g. the on-farm storage of livestock manures) are not considered in this chapter in order to avoid possible double counting. The on-farm storage of livestock manures is dealt with in Chapter 3.B.

ammoniacal nitrogen (TAN) contents. Therefore, it is strongly recommended that digestate is stored in a covered store. The same measures as for livestock manures can be applied for the reduction of NH₃ emissions.

Information on general abatement technologies for NH₃ emissions from storage processes is given in the United Nations Economic Commission for Europe (UNECE) Framework Advisory Code of Good Agricultural Practice for Reducing Ammonia Emissions

(https://www.unece.org/fileadmin/DAM/env/documents/2014/AIR/WGSR/eb.air.wg.5.2001.7.e.pdf) and the draft *Guidance document on preventing and abating ammonia emissions from agricultural sources*

https://www.unece.org/fileadmin/DAM/env/documents/2014/AIR/WGSR/eb.air.wg.5.2001.7.e.pdf). This guidance document also gives information on the emission reduction potential of a variety of abatement technologies in terms of a percentage of unabated storage. If the proportion of digestate stored with certain technologies is known, the emission factor (EF) for this proportion can be reduced by this value.

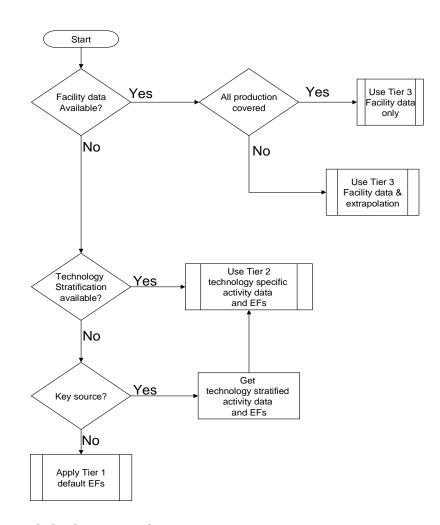
3 Methods

3.1 Choice of method

Figure 3.1 presents the procedure that should be used to select the methods for estimating emissions from this source category. The basic approach is outlined below.

- If detailed information is available, this should be used.
- If the source category is a key category, a Tier 2 or better method must be applied and detailed input data must be collected. The decision tree directs the user in such cases to the Tier 2 method, since it is expected that it will be easier to obtain the necessary input data for this approach than to collect the 'facility level' data needed for a Tier 3 estimate.
- The alternative to applying a Tier 3 method, that is, using a detailed process modelling at facility level, is included under 'facility data' in the decision tree.

Figure 3.1 Decision tree for source category 5.B.2 Biological treatment of waste — anaerobic digestion at biogas facilities



3.2 Tier 1 default approach

3.2.1 Algorithm

The Tier 1 approach estimates the total emission, E_{NH3} (in kg NH₃ per year), from:

$$E_{\rm NH3} = AR_{\rm feedstock} \times EF_{\rm NH3-N, \, Tier\, 1} \times 17/14 \tag{1}$$

where $AR_{feedstock}$ is the total annual amount of N in feedstock, in kg a-¹; and $EF_{NH3-N, Tier 1}$ is the Tier 1 NH₃-N EF related to N in feedstock, in kg NH₃-N per kg N.

3.2.2 Default emission factor

The default EF (Table 3.1) is the total of the Tier 2 EFs provided in section 3.3.2. The range of uncertainty (95 % confidence interval) is estimated in accordance with section 3.3.2.

digestion a	t bioga	s facilities				
		Tier 1 EFs				
	Code	ode Name				
NFR source category	5.B.2	Biological treatment of waste — a	anaerobic	digestion	at biogas facilities	
Fuel	NA					
SNAP (if applicable)	091006	Biogas production				
Technologies/practices						
Region or regional	NA	NA				
conditions						
Abatement technologies	See section 2.4					
Not applicable	As, Cu,	Ni, Se				
Not estimated	NO _x , CO	D, NMVOC, SO ₂ , TSP, PM ₁₀ , PM _{2.5} , BC	, HCB, Pb	, Cd, Hg, C	r, Zn, HCH, PCBs,	
	PCDD/F	⁼ , benzo(a)pyrene, benzo(b)fluorant	hene, ber	nzo(k)fluor	anthene,	
	indeno	(1,2,3-cd)pyrene				
Pollutant	Value	Unit	95	6 %	Reference	
			confi	dence		
	interval					
			Lower	Upper		
NH ₃ -N	0.028	kg NH₃-N per kg N in feedstock	0.0163	0.0501	See text	
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Table 3.1 Tier 1 EFs for source category 5.B.2 Biological treatment of waste — anaerobic digestion at biogas facilities

3.2.3 Activity data

The Tier 1 method requires the total annual amount of N in the feedstock entering the biogas plants to be known. In case this, if data are not available they can be derived from the amount of fresh matter, based on data gathered by statistical surveys or derived from proxy data, e.g. livestock numbers and excretion rates, as well as information (e.g. expert judgement) on the percentage of manure being digested in biogas plants. Table 3.7 provides default factors for the conversion of fresh matter units into N units.

3.3 Tier 2 technology-specific approach

3.3.1 Algorithm

The Tier 2 approach estimates the total emission, *E*_{NH3} (in kg NH₃ per year), from:

$$E_{\rm NH3} = AR_{\rm feedstock} \times \sum_{\rm stages} EF_{\rm NH3-N, \, stage \, i} \times 17/14$$
⁽²⁾

where $AR_{feedstock}$ is the total annual amount of N in feedstock, in kg a-¹; and $EF_{NH3-N, stage1}$ is the NH₃-N EF for stage i (i is the pre-storage, digester, separation of digestate and storage of digestate) related to **N in feedstock**, in kg NH₃-N per kg N.

Note that, according to 2, for each stage the emission is calculated by multiplying the corresponding EF with the total N in the feedstock. This follows from the definition of the EFs (see section 3.3.2).

As pointed out in section 2.3, NH₃ emissions from the digester or the system of digesters can be assumed to be negligible.

As the EFs $EF_{NH3-N, stage i}$ provided in section 3.3.2 are given in relation to N, $AR_{feedstock}$ has to be given in units of N as well. This is a certain drawback of the methodology as NH₃ is in fact related to the

TAN fraction of the total amount of N in the feedstock, rather than the amount of N itself. Countries are encouraged to use, if available, national TAN-related EFs.

3.3.2 Tier 2 emission factors

The European Union (EU) reference document on best available techniques (BREF document) for 'Waste treatment industries' (EC, 2006) gives typical emission ranges for most pollutants, but there is no information for NH₃ emissions. This section presents the Tier 2 NH₃ EFs for anaerobic digestion at biogas facilities adopted from Cuhls et al. (2010). These EFs were derived from trials with municipal organic waste and green waste (gardening waste). For all stages, they were calculated by relating the stage-specific NH₃ emissions (if enclosed, before air scrubbing) to the total amount of fresh matter of the feedstock entering the biogas plants. However, because of the degradation of organic matter during the process, which might vary between the different feedstocks, fresh matter is an inappropriate entity for relating NH₃ emissions to. Hence, the EFs derived by Cuhls et al. (2010) were converted into units of kg NH₃-N per kg N in the feedstock. The input material for the German plants covered by the study of Cuhls et al (2010) are municipal organic wastes and green wastes (gardening wastes). These two substrates are used in approximately equal proportions for biogas production in Germany. Therefore, the arithmetic mean of the N content in fresh matter of municipal organic waste and green waste was used for the conversion. The data are provided in Table 3.7.

 NH_3 emissions from the digester can be considered negligible (see section 2.3), hence an EF of zero is assumed for the digester or the system of digesters.

The EFs for pre-storage, the liquid–solid separation of digestate and the storage of both digestate fractions (Table 3.2 to Table 3.5) describe the emissions without mitigation measures. However, emissions can be reduced by enclosing stages of the process, combined with air scrubbing. For general guidance on abatement technologies, see section 2.4.

Cuhls et al. (2010) do not provide an EF for the storage of non-separated digestate. Therefore, this EF is estimated by adding the EFs for the storage of the two digestate fractions after separation (see Table 3.6). This is possible, as the EFs refer to fresh matter input and therefore are additive. Nevertheless, because of a lack of more detailed information, possible differences in emissions from separated and non-separated digestate, which may arise from differences in the emission-generating processes, are ignored. As both EFs for separated digestate are for open storage, the estimated EF for non-separated digestate applies to open storage as well. Countries are encouraged to use more specific national EFs.

According to Heldstab et al. (2015), p. 284, the uncertainties (95 % confidence interval) of the EFs provided by Cuhls et al. (2010) are estimated to be a factor of 1.75

Table 3.2Tier 2 EFs for source category 5.B.2 Biological treatment of waste — anaerobic
digestion at biogas facilities; pre-storage of feedstock

	Tier 2 EFs					
	Code	Name				
NFR source category	5.B.2	Biological treatment of waste — anaerobic digestion at biogas facilities				
Fuel	NA					
SNAP (if applicable)	091006	Biogas production				
Technologies/practices	Pre-stora	ge				

Region or regional conditions	NA	NA					
Abatement technologies	See section	See section 2.4					
Not applicable	As, Cu, Ni	As, Cu, Ni, Se					
Not estimated	NO _x , CO, NMVOC, SO ₂ , TSP, PM ₁₀ , PM _{2.5} , BC, HCB, Pb, Cd, Hg, Cr, Zn, HCH, PCBs, PCDD/F, benzo(a)pyrene, benzo(b)fluoranthene, benzo(k)fluoranthene, indeno(1,2,3-cd)pyrene						
Pollutant	Value	Unit	95 % Reference confidence interval		Reference		
NH ₃	0.0009	kg NH ₃ -N per kg N in feedstock	Lower 0.0005	Upper 0.0015	See text		

Table 3.3	Tier 2 EFs for source category 5.B.2 Biological treatment of waste — anaerobic
	digestion at biogas facilities; separation of liquid and solid digestate

	Tier 2 EFs						
	Code	Name					
NFR source category	5.B.2	5.B.2 Biological treatment of waste — anaerobic digestion at biogas facilities					
Fuel	NA						
SNAP (if applicable)	091006	Biogas production					
Technologies/practices	Separatio	on of liquid and solid digestate					
Region or regional	NA	JA					
conditions							
Abatement technologies	See section	See section 2.4					
Not applicable	As, Cu, Ni	As, Cu, Ni, Se					
Not estimated	PCDD/F, I	NO _x , CO, NMVOC, SO ₂ , TSP, PM ₁₀ , PM _{2.5} , BC, HCB, Pb, Cd, Hg, Cr, Zn, HCH, PCBs, PCDD/F, benzo(a)pyrene, benzo(b)fluoranthene, benzo(k)fluoranthene, indeno(1,2,3-cd)pyrene					
Pollutant	Value	Unit	confi	% dence rval Upper	Reference		
NH ₃	0.0012	kg NH₃-N per kg N in feedstock	0.0007	0.0020	see text		

Table 3.4Tier 2 EFs for source category 5.B.2 Biological treatment of waste — anaerobic
digestion at biogas facilities; storage of liquid digestate after separation (open
storage)

		Tier 2 EFs		
	Code	Name		
NFR source category	5.B.2	Biological treatment of waste — anaerobic digestion at biogas		
		facilities		
Fuel	NA			
SNAP (if applicable)	091006	Biogas production		
Technologies/practices	Storage of liquid digestate after separation			
Region or regional	NA			
conditions				
Abatement technologies	See section	on 2.4		
Not applicable	As, Cu, N	, Se		
Not estimated	NO _x , CO,	NMVOC, SO ₂ , TSP, PM ₁₀ , PM _{2.5} , BC, HCB, Pb, Cd, Hg, Cr, Zn, HCH, PCBs,		
	PCDD/F,	penzo(a)pyrene, benzo(b)fluoranthene, benzo(k)fluoranthene,		
	indeno(1	2,3-cd)pyrene		

Pollutant	Value	Unit	95 confic inte	dence	Reference
			Lower	Upper	
NH ₃	0.0116	kg NH₃-N per kg N in feedstock	0.0066	0.0202	see text

Table 3.5 Tier 2 EFs for source category 5.B.2 Biological treatment of waste — anaerobic digestion at biogas facilities; storage of solid digestate after separation (open storage)

		Tier 2 EFs					
	Code	Name					
NFR source category	5.B.2	Biological treatment of waste - a	anaerobic	digestion	at biogas facilities		
Fuel	NA						
SNAP (if applicable)	091006	Biogas production					
Technologies/Practices	Storage	of solid digestate after separation					
Region or regional	NA	NA					
conditions							
Abatement technologies	See sect	See section 2.4					
Not applicable	As, Cu, N	As, Cu, Ni, Se					
Not estimated		NMVOC, SO ₂ , TSP, PM ₁₀ , PM _{2.5} , BC					
	-	benzo(a)pyrene, benzo(b)fluorant	nene, ber	120(K)11U01	anthene,		
Pollutant	Value	,2,3-cd)pyrene	05	i %	Reference		
Pollutant	value	Onic			Reference		
		confidence					
		interval					
			Lower	Upper			
NH ₃	0.0150	kg NH₃-N per kg N in feedstock	0.0086	0.0263	See text		

Table 3.6 Tier 2 EFs for source category 5.B.2 Biological treatment of waste — anaerobic digestion at biogas facilities; storage of non-separated digestate (open storage)

		Tier 2 EFs				
	Code	Code Name				
NFR source category	5.B.2	Biological treatment of waste - a	anaerobic	digestion	at biogas facilities	
Fuel	NA					
SNAP (if applicable)	091006	Biogas production				
Technologies/Practices	Storage	of non-separated digestate				
Region or regional	NA	IA				
conditions						
Abatement technologies	See sect	See section 2.4				
Not applicable	As, Cu, N	As, Cu, Ni, Se				
Not estimated	NO _x , CO,	NO _x , CO, NMVOC, SO ₂ , TSP, PM ₁₀ , PM _{2.5} , BC, HCB, Pb, Cd, Hg, Cr, Zn, HCH, PCBs,			r, Zn, HCH, PCBs,	
	PCDD/F,	benzo(a)pyrene, benzo(b)fluorant	hene, ber	nzo(k)fluor	anthene,	
	indeno(1	,2,3-cd)pyrene				
Pollutant	Value	Unit	95	%	Reference	
	confidence					
		interval				
			Lower	Upper		
NH ₃	0.0266	kg NH₃-N per kg N in feedstock	0.0152	0.0465	See text	

3.3.3 Activity data

Surveys on the amounts of different types of feedstock are necessary to derive the necessary activity data on N entering anaerobic digestion. These cover all biodegradable organic materials including livestock manures, crops that are grown for energy production and other organic agricultural wastes,

such as crop residues, that are used for anaerobic digestion at biogas facilities. According to the definition of the EFs (see section 3.3.2), the only the total N amounts of feedstock entering the biogas plants are required for the Tier 2 methodology.

The amounts of N in livestock manures to be digested should be derived from the corresponding N flows calculated in Chapter 3.B, section 3.4.1 (Step 8).

Table 3.7 gives the N contents of some possible feedstock types. These default values can be used to convert feedstock fresh matter into amounts of N. The figures in Table 3.7 are based on German data, but are also in reasonable agreement with data from the United Kingdom (Webb, J., UK national atmospheric emission inventory team, personal communication, 2016). Countries are encouraged to use their own national data if available.

If dry matter contents differ substantially from those given in Table 3.7, N contents can be corrected using the ratio of national to default dry matter contents. In particular, for municipal organic waste, green waste and food waste it is strongly recommended that national data are established, as N content can vary widely.

According to Heldstab et al. (2015), p. 284, the uncertainty of the activity data (95 % confidence interval) is estimated to range from -20 % to +20%.

Feedstock type	Dry matter content of fresh matter (kg kg ⁻¹)	N content of fresh matter (kg kg⁻¹)
Municipal organic waste (ª)	0.40	0.0068
Green waste (grass, etc.) (ª)	Not available	0.0046
Food waste (food processing)	Not available	0.0051
Cattle slurry (ª)	0.10	0.0052
Pig slurry (ª)	0.06	0.0048
Cattle solid manure (^b)	0.25	0.0052
Pig solid manure (^b)	0.25	0.0060
Poultry manure (^b)	0.50	0.0175
Maize silage (ª)	0.35	0.0046
Grass silage (ª)	0.35	0.0094
Straw (ª)	0.86	0.0051

Table 3.7 N content for various feedstock categories

Sources:

(a) KTBL, (2013), (b) LfL (2013).

3.4 Tier 3 emission modelling and use of facility data

This guidebook does not provide a Tier 3 method because of the scarcity of sound methodologies with this approach. However, Wulf and Haenel (2014) proposed a method that could be considered by the countries to implement Tier 3 emission estimates for agricultural feedstock (²). A comprehensive description of this German methodology is given by Haenel et al. (2016).

^{(&}lt;sup>2</sup>)http://www.tfeip-secretariat.org/assets/Ag_Nature/2014/Biogasemission-inventoryTFEIP5.pptx

4 Data quality

4.1 Completeness

A complete inventory for biogas facilities should estimate NH₃, NO, total suspended particles (TSP), particulate matter (PM) and non-methane volatile organic compounds (NMVOCs). However, at present, NO, TSP, PM and NMVOC emissions from biogas facilities cannot be reported, as no methods exist to calculate these emissions.

It is essential to include the complete range of feedstocks in the emission calculations and to ensure that emissions from the utilisation of digestate are reported properly (e.g. utilisation as fertiliser in section 3.D and incineration in Chapter 1.A).

4.2 Avoiding double counting with other sectors

Care should be taken not to double count emissions from biogas facilities. NH₃ emissions resulting from the storage of agricultural feedstocks not located on the premises of biogas facilities have to be considered in Chapter 3.B (Manure management).

In addition, emissions produced from the burning of the biogas produced in engines, boilers and/or turbines have to be reported in the relevant chapter (Chapter 1.A, Combustion).

4.3 Verification

There are no direct methods to evaluate total inventory estimates of NH_3 emissions from the biological treatment of waste.

4.4 Developing a consistent time series and recalculation

There are no specific issues related to developing a consistent time series and recalculation.

4.5 Uncertainty assessment

General guidance on quantifying uncertainties in emission estimates is given in Part A, Chapter 5, 'Uncertainties', of the EMEP/EEA Guidebook (EMEP/EEA, 2016).

The uncertainties related to the EFs are addressed in section 3.3.2. It is good practice to consider that, from country to country, the composition of the treated waste may vary because of differences in waste definitions and fractionation. This could lead to country-specific EFs that are not comparable with those of other countries.

For more on the uncertainty of the activity data, see section 3.3.3.

4.6 Inventory quality assurance/quality control (QA/QC)

There are no specific issues related to inventory quality assurance/quality control (QA/QC).

4.7 Gridding

There are no specific issues related to gridding.

4.8 Reporting and documentation

Emissions calculated with Equations 1 or 2 are to be reported under NFR 5.B.2.

It should be noted that emissions from the application of digestate to land need to be reported under NFR 3.D.a.2.c.

Documentation, detailing when and where the biogas facility inventory was checked and by whom, is required.

5 References

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6 Point of enquiry

Enquiries concerning this chapter should be directed to the relevant leader(s) of the Task Force on Emission Inventories and Projections' (TFEIP's) Expert Panel on combustion and industry. Please refer to the TFEIP website (<u>www.tfeip-secretariat.org/</u>) for the contact details of the current expert panel leaders.